

Simulation of Multi-Stage Flash with Brine Circulating Desalination Plant

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Abstract

Multi-stage flash (MSF) desalination is the main process to solve the problem of limited freshwater resources in the world. This work describes the developed steady-state mathematical model for analysing and evaluating the performance of Multistage flashing with brine circulation desalination process (MSF-BC). It is based on the laws of energy balance, material balance, and heat transfer equations with physical properties correlations equations. The nonlinear equations are linearized and arranged into a tridiagonal matrix form. The model solution is obtained by a computer code written by MATLAB program software. It can predict the productivity of the plant with temperature profiles and flow rates for all stages in the unit. The model results were compared with some previous results presented in literature. The comparison shows good agreement with these available data. An MSF desalination plant in Ayoun Mousa, Egypt of capacity 5000 m³/day was presented as a case study.

Keywords

Steady-state modelling;
System of non-linear
equations;Tri-diagonal
matrix; System
performance; Multi-stage
Flash Desalination.

Introduction

Water plays an important role in all aspects of life including industrial activities. Drinking water is unfairly similar to most other natural resources, which are distributed unequally around the world.

There is increasing worldwide concern about the scarcity of global water resources, day by day. So, desalination of seawater became a major solution for providing arid zones with continuous supply of fresh water.

Multi-stage flash desalination (MSF) is one of the major methods for the desalination industry with a market share of around 60% of the total production capacity worldwide (1).

The MSF desalination process is based on flash evaporation, depends on using vaporization through multi-stage chambers. The MSF desalination process has many advantages such as it can produce high quality of freshwater with TDS of less than 30 ppm. The produced water can be used in many purposes like boiler making water, chemical processes, dairy and food washing, cooling and cleaning (2). Besides the high-water quality, it produces large quantities of fresh water up to 75000 m³/d for each unit.

The MSF desalination plants are composed of two models (3), Once-through MSF (MSF-OT) which consist of two sections (brine heater and heat recovery sections) and

Brine recirculation MSF (MSF-BC) which has one extra section (heat rejection section).

Many researches were conducted to enhance the operation of MSF desalination plants as efficiently as possible and, as a result, to reduce the cost of water generated from such plants. Part of this work focuses on mathematical modelling as a cheap alternative for industrial scale applicative. Models of MSF process can be classified into two different categories; Steady state models (simple and rigorous) and dynamic models.

The steady state mathematical model of MSF-BC process that based on the basic laws of thermodynamics is established in the literature. Models can sort from simple steady-state models with constant thermophysical properties of fluid streams (4; 5; 6; 7; 8; 9) to rigorous mathematical models which taking into account the variation of the thermo-physical properties of various fluids with temperature and salinity (10; 11; 12; 13; 14; 15; 16; 17; 18; 19). (20; 21; 22; 23; 24)

The main aim of this paper is to provide an algorithm for solving the large system of algebraic and nonlinear equations which is a rigorous steady-state mathematical model for MSF-BR. The system will be solved through Linearizing the equations into tri-diagonal matrix form (TDM) using MATLAB software. The results were verified against previous simulation data given by Abdul Wahab, (2012) (25), In addition, we studied the performance of actual desalination plant of Ayoun Mousa, Egypt (26).

Process Description

The MSF process with brine circulation is shown in Figure 1 (21). The process is divided into three sections: the brine heater, the heat recovery and the heat rejection sections. Stages of heat recovery include heating of the recycled brine stream inside the condenser tubes from the brine blowdown temperature to a higher temperature near to the top brine temperature. So, the amount of steam used in the brine heater is minimized. The heat rejection section consists of three stages. The function of the heat rejection section is to monitor the feed seawater temperature and reject the excess heat added in the brine heater. Feed seawater enters the last stage of the heat rejection section (F_{sea}) and move through the condenser tubes to remove heat from the stages. The stream leaving the first stage of the heat rejection section is separated into two streams; the rejected seawater (C_w) and the makeup stream (F) which is mixed with recycled brine (R) from the last stage of the heat rejection section. Cooling brine (W) enters the last stage of the heat recovery section. It heats gradually by the flashing brine in each stage and leaves the heat recovery section from the first stage. Then it enters the brine heater to raise its temperature to the top brine temperature (TBT) and enters into the 1st flashing stage and produce flashing vapor. This continuous till the last stage of the heat rejection section. The brine stream (B_N) from the last stage is split into two streams: the blowdown (BD) stream that is settled to the sea and the remaining recycled water stream (R) which is recycled back to mix with the makeup flow. The distillate is collected from each stage to produce the freshwater product at the end (D_N).

Mathematical Model

The following simplifying assumptions were used in the rigorous steady state modelling,

- Steady_state_operation is the common assumption amongst all studies. (18) .
- The distillate is free from salt.
- Heat losses to the surroundings are insignificant.
- Brine holdup and brine flow rate are considered as constant along the unit.
- Heat transfer area shall be considered the same for each part of the plant.
- The physical_properties such as heat capacity, viscosity, brine densities, boiling temperatures, vapor enthalpy temperature, and heat transfer coefficient depend on temperature and salinity variation.
- Thermodynamic losses include the boiling point elevation (BPE), the non-equilibrium allowance (NEA), and demister losses (DEM).
- The effect of non-condensable gases on heat transfer is negligible.

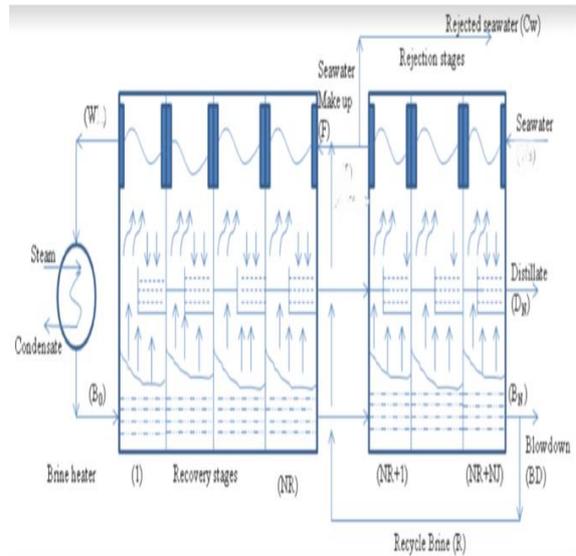


Figure 1: Multistage Flash Desalination Brine process circulation (MSF-BC)

- Heat from mixing is negligible due to the low NaCl heat of mixing

The steady-state model equations consist of a set of energy and material balance equations which include the following (25):

- Overall material balance equations.
- Material balance equation for each stage.
- Salt_balance_equation for each stage.
- Enthalpy balance equations on flashing brine
- Overall enthalpy balance for any stage.
- Brine heater model.
- Mixing and splitting equations.

Schematics of the MSF variables in the flashing_stage_and the_brine_heater are shown in Figures 2 and 3 (21).

Overall Material Balance Equations

As shown in Figure 1 (21), the overall mass balance for MSF desalination plant is given by,

$$F_{sea} = C_w + D_N + B_N \quad (1)$$

The material balance for the splitter is given by,

$$C_w = F_{sea} - F \quad (2)$$

Substituting Equation 2 into Equation 1 yields,

$$F + D_N + B_D \quad (3)$$

The overall material balance for the MSF plant as shown in Equation 3 has one input stream and two output streams. The overall salt balance is given by,

$$FX_F = B_D X_{BN} \quad (4)$$

It should be noticed that the Equation 4 assumes that the distillate is free from salt.

Material and Salt Balance Equations for Each Stage

The summation of the inlet flashing brine and distillate flow rates will be equal to the summation of those streams leaving the stage (j).

Mass Balance in the flash chamber

$$B_{j-1} + D_{j-1} = B_j + D_j \quad (5)$$

Stage salt balance:

$$B_{j-1}X_{Bj-1} = B_jX_{Bj} \quad (6)$$

Mass balance for distillate tray

$$\sum_{K=1}^j D_k = \sum_{K=1}^{j-1} D_k + D_j \quad (7)$$

Enthalpy Balance Equations on Flashing Brine

For the flashing brine at stage (j), the enthalpy balance equation is given by,

$$B_{j-1}h_{Bj-1} = B_jh_{Bj} + (B_{j-1} - B_j)h_{vj} \quad (8)$$

Overall Enthalpy Balance for Any Stage

For a steady-state operation, the summation of the enthalpies of all input streams for stage (j) should be equal to the summation of all streams leaving the stage. There is no generation or accumulation of energy in the stage. The overall enthalpy balance for any stage (j) is given by:

$$\begin{aligned} WS_{Rj}(T_{Fj} - T_{Fj+1}) = & \quad (9) \\ D_{j-1}S_{Dj-1}(T_{Dj-1} - T^*) + & \\ B_{j-1}S_{Bj-1}(T_{Bj-1} - T^*) - & \\ D_jS_{Dj}(T_{Dj} - T^*) - B_jS_{Bj}(T_{Bj} - T^*) & \end{aligned}$$

Where,

The specific heat capacity of pure saturated water (SDj) (29) is given by,

$$\begin{aligned} S_{Dj} = & \quad (10) \\ 1.001183 - & \\ 6.61666652 * 10^{-5}T_{Dj} + & \\ 1.3999989 * 10^{-7}T_{Dj}^2 + & \\ 1.3333336 * 10^{-9}T_{Dj}^3)4.184 & \end{aligned}$$

The specific heat capacity of flashing brine at each stage (SBj) (29) given by,

$$\begin{aligned} S_{Bj} = & \quad (11) \\ 4.185 - 5.381 * & \\ 10^{-3}X_{Bj} + 6.26 * 10^{-6}X_{Bj}^2) - & \\ (3.055 * 10^{-5} + 2.774 * & \end{aligned}$$

$$\begin{aligned} 10^{-6}X_{Bj} - 4.318 * 10^{-8}X_{Bj}^2)T_{Bj} + & \\ (8.844 * 10^{-7} + 6.527 * & \\ 10^{-8}X_{Bj} - 4.003 * 10^{-10}X_{Bj}^2) & \end{aligned}$$

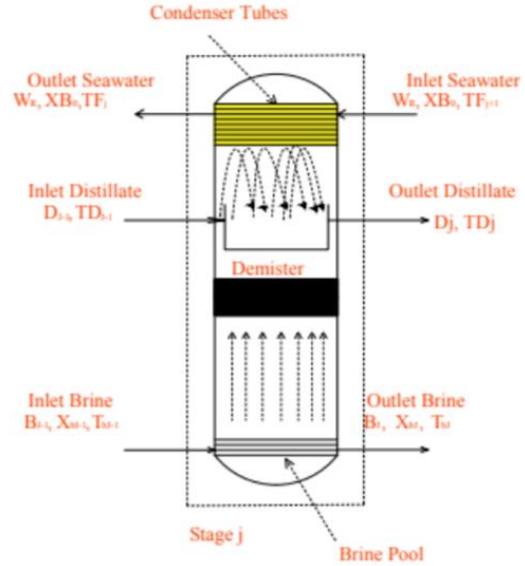


Figure 2: A general stage in an MSF plant

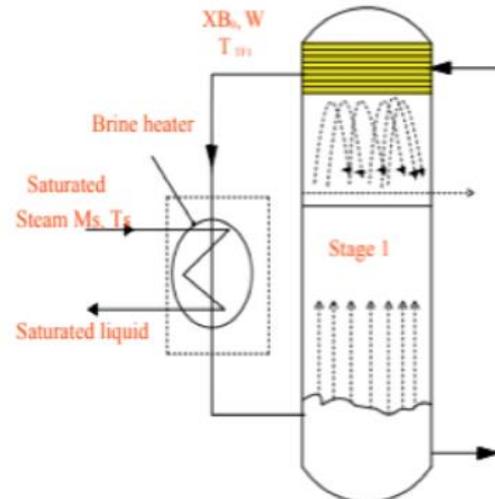


Figure 3: Typical brine heater

Heat Transfer Equation

The heat transferred to the cooling condenser tubes owing to condensation of the flashed vapor in stage(j). Heat transfer equation in the heat recovery section is given by:

$$WS_{Rj}(T_{Fj} - T_{Fj+1}) = U_jA_jLMTD_j \quad (12)$$

In the heat rejection section, replacing W instead of Fsea. The logarithmic mean temperature difference in the recovery and rejection stages.

$$LMTD_j = (T_{Fj} - T_{Fj+1}) / \ln \left\{ \frac{T_{Dj} - T_{Fj+1}}{T_{Dj} - T_{Fj}} \right\} \quad (13)$$

Equilibrium Equation

The distillate and flashing brine temperature correlation is given by,

$$T_{Bj} = T_{Dj} + BPE + NEA + DEM \quad (14)$$

Where,

Boiling Point Elevation (28)

The boiling point elevation correlation of seawater is given by,

$$BPE = AX + BX^2 + CX^3 \quad (15)$$

$$A = (8.25 * 10^{-2} + 1.883 * 10^{-4}T + 4.02 * 10^{-6}T^2) \quad (16)$$

$$B = (-7.625 * 10^{-4} + 9.02 * 10^{-5}T - 5.2 * 10^{-7}T^2) \quad (17)$$

$$C = (1.522 * 10^{-4} - 3 * 10^{-6}T - 3 * 10^{-8}T^2) \quad (18)$$

Where X is the weight percentage of the salt and T is the temperature in °C.

Non-equilibrium allowance (28)

The NEA correlation for the MSF system is given by,

$$NEA = \left(\frac{NEA_{10}}{0.5\Delta T + NEA_{10}} \right)^{0.3281L} (0.5\Delta T + NEA_{10}) \quad (19)$$

$$NEA_{10} = (0.9784)^{Ti} (15.7378)^H (1.3777)^{Vb * 10^{-6}} \quad (20)$$

Demister and Other Losses (31)

The temperature loss that follows the pressure drop through the demister and condenser tubes is calculated from the following equation:

$$DEM = \frac{\exp(1.885 - 0.02063(1.8T_{Dj} + 32))}{1.8} \quad (21)$$

The distillate flashed steam temperature correlation is given by,

$$T_{vj} = T_{Dj} + DEM \quad (22)$$

Brine Heater Model

As shown in the Figure 4, the performance of brine heater can be described as

Mass balance (brine):

$$W = B_o \quad (23)$$

Overall enthalpy balance:

$$B_o S_{Rj} (T_{Bo} - T_{F1}) = M_s \lambda_s \quad (24)$$

Where,

The latent heat of vaporization (28) is given by,

$$\lambda_s = 2501.897149 - 2.407064037T + 1.192217 * 10^3 T^2 - 1.5863 * 10^5 T^3 \quad (25)$$

Heat transfer equation in the brine heater:

$$WS_{RH} (T_{Bo} - T_{F1}) = U_H A_H LMTD_H \quad (26)$$

The heat transfer coefficient for the brine and vapor side (31) is given by,

$$U = \frac{4.8857}{y + z + 4.8857 F_{jj}} \quad (27)$$

Where,

$$z = 0.102 * 10^{-2} - 0.747 * 10^{-5} T_{Dj} + 0.997 * 10^{-7} T_{Dj}^2 - 0.430 * 10^{-9} T_{Dj}^3 + 0.620 * 10^{-12} T_{Dj}^4 \quad (28)$$

$$y = \frac{(V_{Bj} I D_j)^{0.2}}{(160 + 1.92 T_{Bj}) V_{Bj}} \quad (29)$$

The logarithmic mean temperature difference for the brine heater (LMTD_j)

$$LMTD_H = (T_{Bo} - T_{F1}) / \ln \left\{ \frac{T_s - T_{F1}}{T_s - T_{Bo}} \right\} \quad (30)$$

Mixer and Splitter Model

Mass balance on mixer:

$$W = F + R \quad (31)$$

Salt balance on mixer:

$$WX_{Bo} = FX_F + RX_{BN} \quad (32)$$

Enthalpy balance on mixer:

$$Ce = c_{3j} + 1 \quad (41)$$

$$Wh_M = Rh_R + Fh_F \quad (33)$$

$$De = -b_{3j} \quad (42)$$

At splitting point:

$$B_D = B_N - R \quad (34)$$

Where,

$$c_{1j} = -\left(\frac{b_{1j} \alpha_{j-1}}{1 - \alpha_{j-1}}\right) \quad (43)$$

Where,

$$c_{2j} = \left(\frac{b_{1j}}{1 - \alpha_{j-1}}\right) - \left(\frac{b_{2j} \alpha_j}{1 - \alpha_j}\right) \quad (44)$$

The specific enthalpy of saturated water (30) is given by,

$$h_{Dj} = (1.001183T_{Dj} - 3.0833326 * 10^{-5}T_{Dj}^2 + 4.666663 * 10^{-8} * T_{Dj}^3 + 3.333334 * 10^{-10}T_{Dj}^4 - 31.92)\left(\frac{4.184}{1.8}\right) \quad (35)$$

$$c_{3j} = \frac{b_{2j}}{1 - \alpha_j} \quad (45)$$

The water vapor enthalpy is given by,

$$h_v = 2499.15 + 1.955T - 1.927 * 10^{-3}T^2 \quad (36)$$

$$b_{1j} = a_{1j} + a_{2j} \quad (46)$$

$$b_{2j} = -(a_{3j} + a_{4j}) \quad (47)$$

$$b_{3j} = a_{5j} + a_{2j}Z_{j-1} - a_{4j}Z_j \quad (48)$$

The specific enthalpy of brine at each stage given by,

$$h_{Bj} = (4.185 - 5.381 * 10^{-3}X_{Bj} + 6.26 * 10^{-6}X_{Bj}^2)T_{Bj} - (3.055 * 10^{-5} + 2.774 * 10^{-6}X_{Bj} - 4.318 * 10^{-8}X_{Bj}^2)T_{Bj}^2 + (8.844 * 10^{-7} + 6.527 * 10^{-8}X_{Bj} - 4.003 * 10^{-10}X_{Bj}^2)T_{Bj}^3 \quad (37)$$

Where,

$$\alpha_{1j} = \frac{D_{j-1} * S_{Dj-1}}{W * S_{Rj}} \quad (49)$$

$$\alpha_{2j} = \frac{B_{j-1} * S_{Bj-1}}{W * S_{Rj}} \quad (50)$$

$$\alpha_{3j} = \frac{D_j * S_{Dj}}{W * S_{Rj}} \quad (51)$$

$$\alpha_{4j} = \frac{B_j * S_{Bj}}{W * S_{Rj}} \quad (52)$$

Solution of the Systems of Equations

The above mentioned equations composed of algebraic and nonlinear equations. The linearization of MSF-BC plant equations suggested by Helal et al. (10), into tri-diagonal matrix arrangement (TDM form) was selected in this work since this approach has the following advantages (26):

- The algorithm has high degree of convergence stability and results in shorter run times compared with calculation approaches which follow stage wise.
- Small number of iterations required

The final form of TDM for stage(j) in the recovery and rejection sections is:

$$Ay_j T_{Fj-1} + Be_j T_{Fj} + Ce_j T_{Fj+1} = De_j \quad (38)$$

Where,

$$Ay = c_{1j} \quad (39)$$

$$Be = c_{2j} - 1 \quad (40)$$

The mathematical model for a steady state process, as described above, is used to build MATLAB code for performance analysis of MSF desalination systems. Figure 4 gives the flow chart of the model solution steps used for steady state simulation of the MSF desalination systems by tridiagonal matrix.

Model Validation

Figures (5 and 6) Compare the temperatures of the flashing brine (TBj), distillate (TDj), and recirculating brine (TFj) in 24 flashing stages of simulation results reported by Abdul Wahab, (2012) (25) based on Barka MSF desalination plant data with values predicted by developed model. The results show a good agreement.

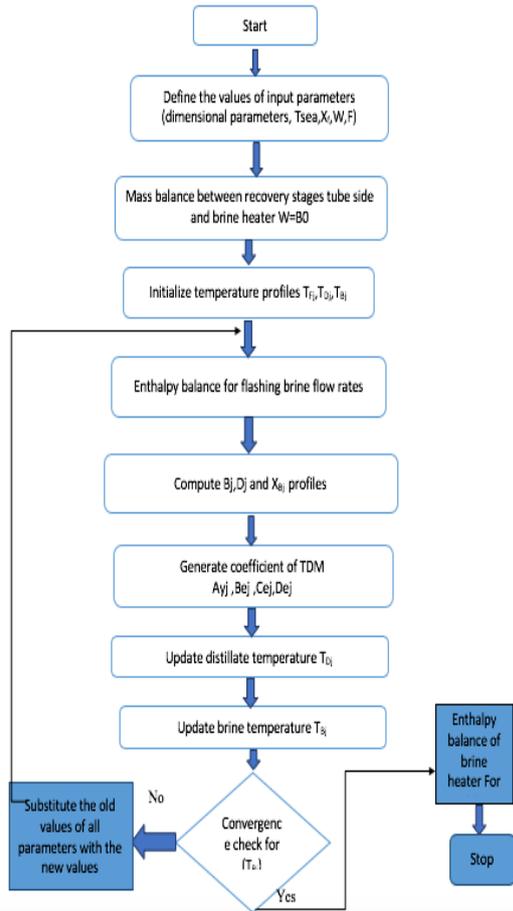


Figure 4: The flow chart for the solution of the developed model (TDM)

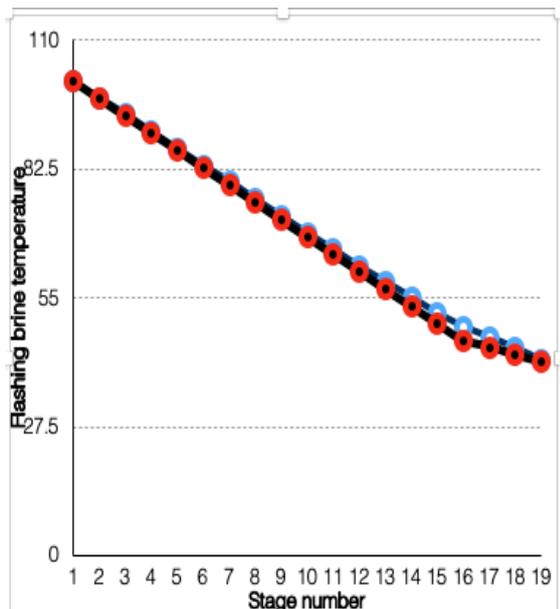


Figure 5: Comparison of our work with Abdel-wahab(2012) for flashing stage temperature(TBj)

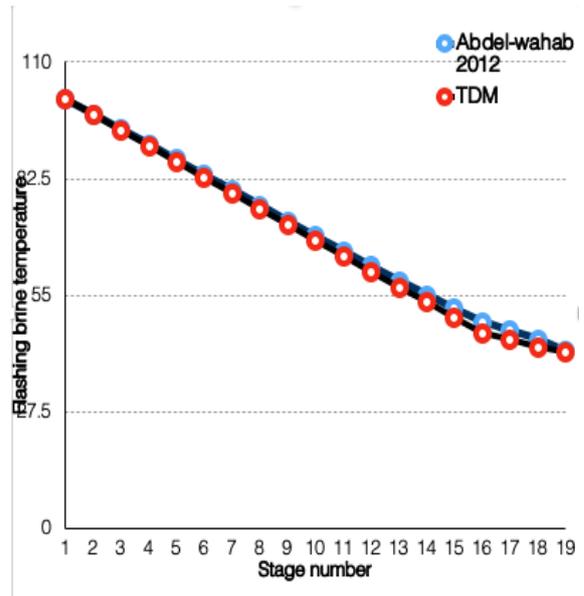


Figure 6: Comparison of our work with Abdel-wahab(2012) for distillate temperature(TDj)

Results

The presented model was useful to simulate the production of Ayoun Mousa MSF plant in Egypt. The capacity of the unit is 5000 m³/day and the operating conditions are listed in Table 1 (27). Initial guessing values of the mass flow rates and the temperatures of all the process streams were obtained from simple mathematical model suggested by El-Dessouky and Ettouney (2002)(28). After demonstrating the capability of the developed model, it is used to measure the productivity with the profiles of temperatures and flow rates in all the stages of the unit. The simulation results for the operating parameters of this work is shown in the Table 2.

Table 1: Design and operational data for Ayoun Mousa MSF desalination plant.

5000 m ³ /day MSF_BC	
Top brine temperature (TBT) °C	110
Brine blowdown temperature °C	39
Feed seawater temperature °C	27
Cooling water splitter ratio	0.482
Sea water salinity, ppm	48000
Brine blow down salinity, ppm	70000
Number of stages	20(N _R =17, N _J =3)
Brine load Kg/m.s	180
Vapor velocity m/s	12
Weir coefficient Cd	0.5
Tube outside diameter, m	0.02199
Tube inside diameter, m	0.01949
BH outside diameter, m	0.0239
BH inside diameter, m	0.0214

Table 2: Model predictions for this operating condition of this work.

j	T _{Bj} , °C	T _{Dj} , °C	T _{Fj} , °C	B _j kg/s	D _j kg/s	X _j wt%
1	106.45	105.28	102.7147	480.25	3.071	62.46
2	102.9	101.671	99.1212	477.22	6.122	62.86
3	99.3	98.0601	95.4894	474.207	9.154	63.26
4	95.62	94.3652	91.7873	471.213	12.167	63.66
5	91.96	90.6857	88.1119	468.238	15.1619	64.067
6	88.27	86.9711	84.41	465.281	18.137	64.474
7	84.59	83.2607	80.7182	462.344	21.0935	64.884
8	80.9	79.5337	77.0136	459.424	24.0312	65.296
9	77.22	75.8092	73.3136	456.524	26.9504	65.711
10	73.56	72.0963	69.6264	453.641	29.851	66.128
11	69.91	68.3938	65.9503	450.777	32.733	66.549
12	66.32	64.7006	62.2843	447.931	35.597	66.971
13	62.73	61.0455	58.6578	445.103	38.444	67.397
14	59.24	57.4172	55.0606	442.203	41.272	67.825
15	55.73	53.8345	51.5128	442.292	44.0826	68.256
16	52.26	50.1963	47.9148	439.552	46.8752	68.69
17	48.85	45.18	43.81	436.725	49.6549	69.126
18	45.38	43.1933	40.8367	433.967	52.407	69.565
19	42.36	40.0599	37.7382	431.227	55.1476	70.008
20	39.47	37.17	34.8885	428.504	57.8752	70.452

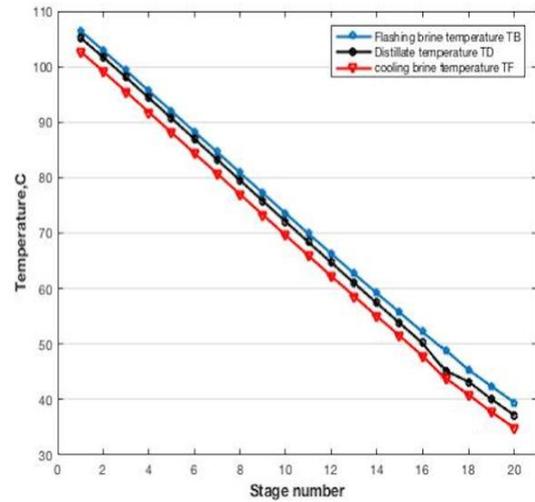


Figure 7: Temperature variation through the stages.

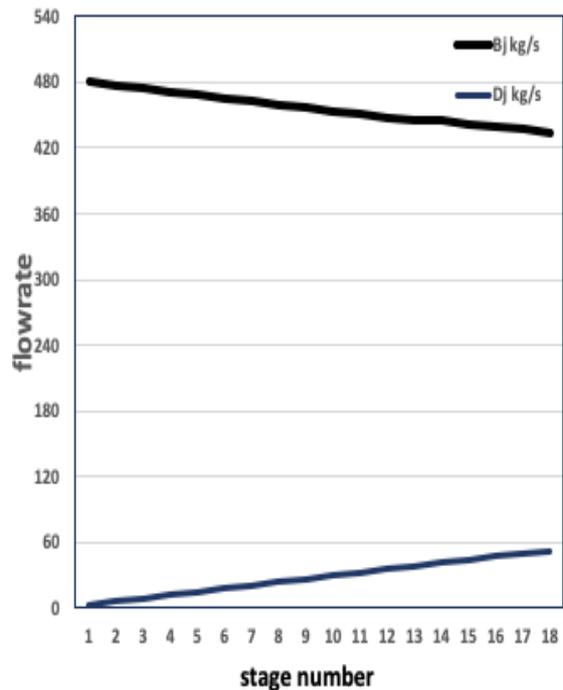


Figure 8: Flowrates variation through the stages.

As shown in Figures (7 and 8) because of the flashing cycle, the outlet brine temperature is decreasing. In addition, the brine flow rate is decreasing due to the distillate formed in each stage. Furthermore, the salinity of the product decreases across the stages. That is because the distillate is almost salt free compared to the brine.

Conclusions

Steady-state models are useful for evaluating the plant operating conditions; studying the performance of plant. They also provide traces for improving the plant efficiency. The developed model can be used to analyze the MSF-BC desalination process at steady state operation conditions. The developed MATLAB code can be used to perform the performance analysis of MSF-BC desalination plants by calculating the productivity of the plant with profiles of temperatures and flow rates in all stages of the unit. The developed model is valid when compared with commercial software used for the same purpose. The presented model predictions were compared with vendor

simulation results for BARKA MSF desalination plant reported by Abdul Wahab, (2012), and There was a satisfactory matching between them. Ayoun Mousa MSF desalination plant located in Egypt was used as a case study to predict the performance of the plant.

Nomenclature

A	Heat transfer area, m ²
BD	Blow-down mass flow rate, Kg/s
BN	Flashing brine mass flowrate leaving stage N, Kg/s
BPE	Boiling point elevation
C _w	Rejected seawater mass flowrate, Kg/s
DEM	Temperature losses due to demister, °C
D	diameter of tube, m
DN	Distillate flowrate leaving stage N, Kg/s
F	Make-up seawater mass flow rate, Kg/s
F _{sea}	Intake seawater mass flow rate, Kg/s
h	Specific enthalpy, Kcal/Kg
L	Length of tubes, m
NEA	Non-equilibrium allowance
R	Recycled brine mass flow rate, Kg/s
S	Specific heat capacity, Kcal/Kg °C
T	Temperature, °C
TBT	Top brine temperature, °C
U	Overall heat transfer coefficient, Kcal/m ² h K
W	Cooling brine mass flow rate leaving stage 1, Kg/s
X	Salinity, wt. %
λ _s	Latent heat of steam to the brine heater, Kcal/Kg
F _{Fj}	Fouling factor at stage j (h m ² °C/Kcal)
V _{bj}	Linear velocity of brine stream (ft/s)

Subscripts

b	brine
D	Distillate product
H	Brine heater
j	Stage number
N	Last stage of the unit
R	Recycled brine stream

References

- 1- El-Dessouky, H. T., & Ettouney, H. M. (2002). Fundamentals of salt water desalination. Elsevier.
- 2- Hilal, N., Kim, G. J., & Somerfield, C. (2011). Boron removal from saline water: a comprehensive review. *Desalination*, 273(1), 23-35.
- 3- Nair, M., & Kumar, D. (2013). Water desalination and challenges: the Middle East perspective: a review. *Desalination and Water Treatment*, 51(10-12), 2030-2040. Vols. 51, 2030-2040.
- 4- Mandil, M. A., & Ghafour, E. A. (1970). Optimization of multi-stage flash evaporation plants. *Chemical Engineering Science*, 25(4), 611-621.
- 5- Coleman, A. K. (1971). Optimization of a single effect, multi-stage flash distillation desalination system. *Desalination*, 9(4), 315-331.
- 6- Soliman, M. A. (1981). A mathematical-model for multistage flash desalination plants. *Journal of Engineering Sciences*, 7(2), 143-150.
- 7- Darwish, M. A. (1991). Thermal analysis of multi-stage flash desalting systems. *Desalination*, 85(1), 59-79.
- 8- El-Dessouky, H., Alatiqi, I., & Ettouney, H. (1998). Process synthesis: the multi-stage flash desalination system. *Desalination*, 115(2), 155-179.
- 9- Al-bahou, M., Al-Rakaf, Z., Zaki, H., & Ettouney, H. (2007). Desalination experience in Kuwait. *Desalination*, 204(1-3), 403-415.
- 10- Helal, A. M., Medani, M. S., Soliman, M. A., & Flower, J. R. (1986). A tridiagonal matrix model for multistage flash desalination plants. *Computers & chemical engineering*, 10(4), 327-342.
- 11- Hussain, A., Hassan, A., Al-Gobaisi, D., Al-Radif, A., Woldai, A., & Sommariva, C. (1993). Modeling, simulation, optimization and control of multistage flash (MSF) desalination plants Part2: Modeling and simulation. *Desalination*, 92, 21-41.
- 12- Aly, S.E. and Fathalah, K. (1995). MSF - a mathematical model, Proc. IDA World Congress, Abu Dhabi, 203-226.
- 13- El-Dessouky, H., Shaban, H. I., & Al-Ramadan, H. (1995). Steady-state analysis of multi-stage flash desalination process. *Desalination*, 103(3), 271-287.
- 14- Rosso, M., Beltramini, A., Mazzotti, M., & Morbidelli, M. (1997). Modeling multistage flash desalination plants. *Desalination*, 108(1-3), 365-374.
- 15- Thomas, P. J., Bhattacharyya, S., Patra, A., & Rao, G. P. (1998). Steady state and dynamic simulation of multi-stage flash desalination plants: A case study. *Computers & chemical engineering*, 22(10), 1515-1529.
- 16- Aly, N. H., & El-Figi, A. K. (2003). Thermal performance of seawater desalination systems. *Desalination*, 158(1-3), 127-142.
- 17- Tanvir, M. S., & Mujtaba, I. M. (2006). Modelling and simulation of MSF desalination process using gPROMS and neural network based physical property correlation. *Computer aided chemical engineering*, 21(A), 315.
- 18- Abdel-Jabbar, N. M., Qiblawey, H. M., Mjalli, F. S., & Ettouney, H. (2007). Simulation of large capacity MSF brine circulation plants. *Desalination*, 204(1-3), 501-514.
- 19- Alasfour, F. N., & Abdulrahim, H. K. (2009). Rigorous steady state modeling of MSF- BR desalination system. *Desalination and Water Treatment*, 1(1-3), 259-276.

- 20- Hawaidi, E. A., & Mujtaba, I. M. (2010). Sensitivity of brine heater fouling on optimization of operation parameters of MSF desalination process using PROMS. In 20th European Symposium on Computer Aided Process Engineering-ESCAPE20.
- 21- Said, S. A. R. (2013). MSF process modelling, simulation and optimisation: impact of non-condensable gases and fouling factor on design and operation.(Doctoral dissertation, University of Bradford.
- 22- Ali, M. B., & Kairouani, L. (2014). Solving equations describing the steady-state model of MSF desalination process using Solver Optimization Tool of MATLAB software. *Desalination and Water Treatment*, 52(40-42), 7473-7483.
- 23- Al-Hamahmy, M., Fath, H. E., & Khanafer, K. (2016). Techno-economical simulation and study of a novel MSF desalination process. *Desalination*, 386, 1-12.
- 24- Wael.A.(2017, september).Modelling and Simulation of Multistage Flash Desalination Plants.In *Libyan Journal for Engineering Research (LyJER)*,ISSN 2522- 6967.
- 25- Al-Shayji, K. A. M. (1998). Modeling, simulation, and optimization of large-scale commercial desalination plants (Doctoral dissertation, Virginia Tech).
- 26- Abdul-Wahab, S. A., Reddy, K. V., Al-Weshahi, M. A., Al-Hatmi, S., & Tajeldin, Y. M. (2012). Development of a steady-state mathematical model for multistage flash (MSF) desalination plant. *International Journal of Energy Research*, 36(6), 710-723.
- 27- Nafey, A. S. (2005). Simulation of solar heating systems—an overview. *Renewable and Sustainable Energy Reviews*, 9(6), 576-591.
- 28- Ettouney, H., El-Dessouky, H., & Al-Juwayhel, F. (2002). Performance of the once- through multistage flash desalination process. *Proceedings of the Institution of Mechanical Engineers, Part A: Journal of Power and Energy*, 216(3), 229-241. Vols. 229-242 (2).
- 29- Helal, A. M., El-Nashar, A. M., Al-Katheeri, E., & Al-Malek, S. (2003). Optimal design of hybrid RO/MSF desalination plants Part I: Modeling and algorithms. *Desalination*, 154(1), 43-66.
- 30- Perry, R. H., Green, D. W., & Maloney, J. O. (1997). *Perry's chemical engineers' handbook*.
- 31- Rosso, M., Beltramini, A., Mazzotti, M., & Morbidelli, M. (1997). Modeling multistage flash desalination plants. *Desalination*, 108(1-3), 365-374.